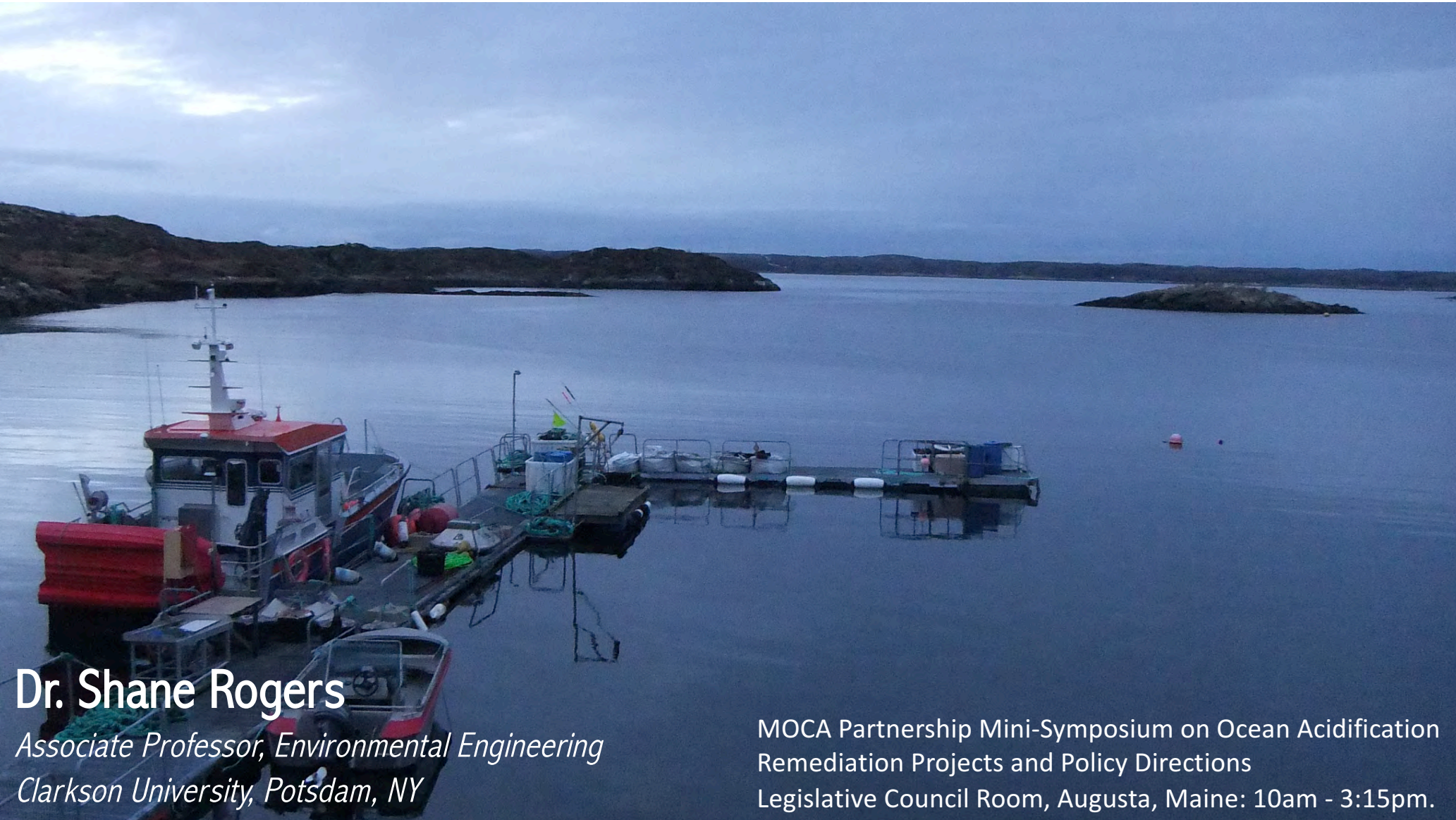


# Nutrient Bioextraction and Bioenergy Recovery from Ocean Outfalls of Treatment Works



**Dr. Shane Rogers**

*Associate Professor, Environmental Engineering  
Clarkson University, Potsdam, NY*

MOCA Partnership Mini-Symposium on Ocean Acidification  
Remediation Projects and Policy Directions  
Legislative Council Room, Augusta, Maine: 10am - 3:15pm.



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Shane W Rogers

Abstract Number: OR-19-04

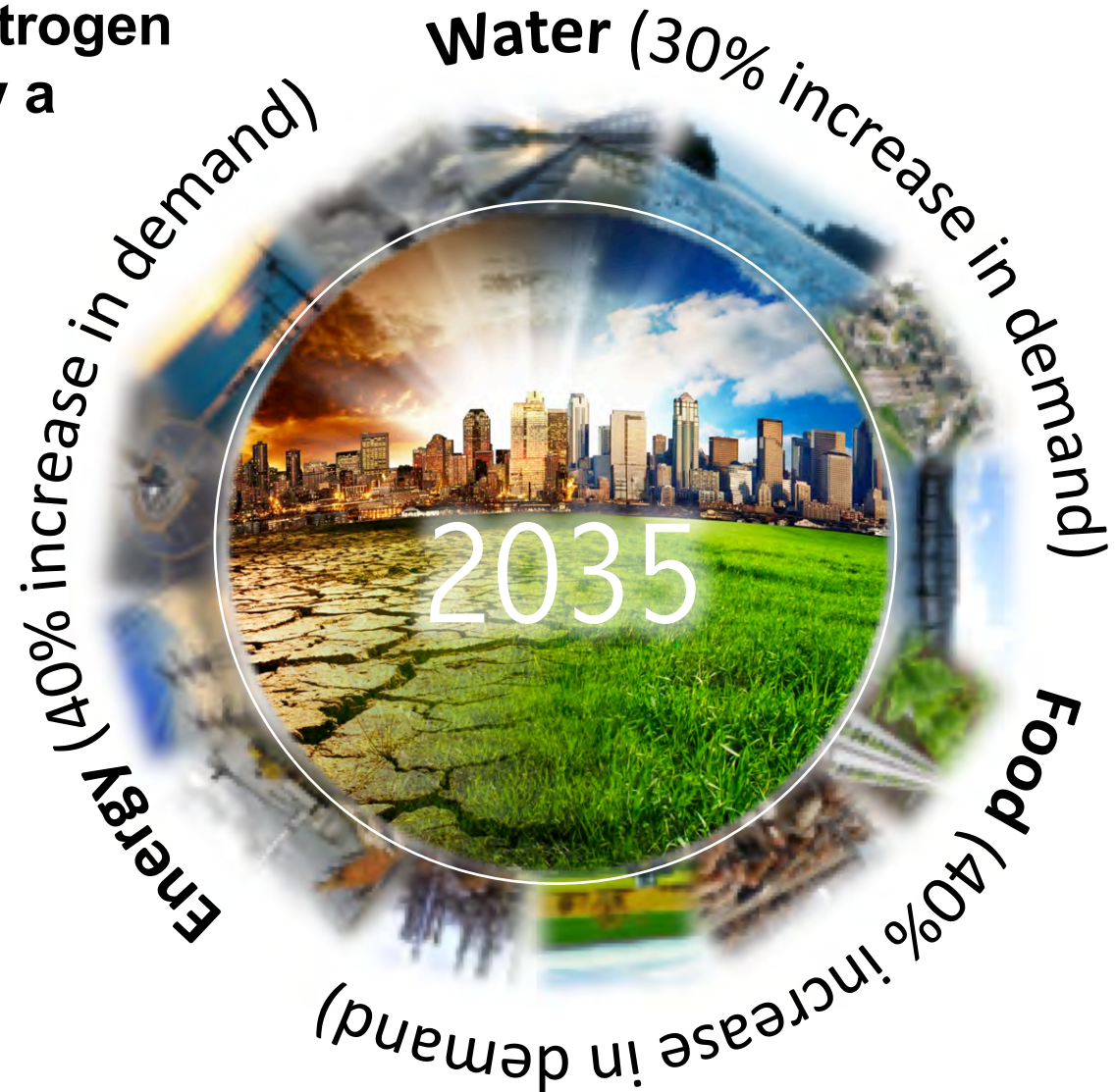
Session title: OR-19-IMTA and Biomitigation (minisym)

As global populations soar, we face unparalleled challenges of food, water, and energy security and sustainability.

Improved management of the nitrogen and phosphorus cycles will play a central role in this challenge.



**Increasing population**  
**Urbanization & Modernization**  
**Rightful Goal of Poverty Alleviation**  
**Changing global climate**  
**Eutrophication**



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## Consider:

- 15M tons  $\text{NH}_3$  produced in the US in 1999 using Haber process (from atmospheric N)
  - Consumed 3% of the total US natural gas production in 1999
  - >90% of the  $\text{NH}_3$  produced was for the fertilizer industry
- ~140M tons  $\text{NH}_3$  fertilizer are produced globally, >99% by the Haber process

## $\text{NH}_3$ produced has had profound impact on our global societies:

- Supports bioenergy feedstock, feed, and food that sustains 60% of global populace
- Population explosion of the last 150 years would not otherwise have been possible
- ~ 80% of N in modern human tissues is likely to have originated from Haber process

## ...and sustainability of our global environment:

- Nutrient runoff from terrestrial production of food, feed, and bioenergy feedstock degrades water quality and damages freshwater and coastal water ecosystems
- These ecosystems are further stressed by increased temperature and acidification caused by greenhouse gases released by agriculture and combustion of fossil fuels for energy and fertilizer N production.

Global use of nitrogen fertilizers produced by the Haber process is increasing at a rate of approximately 15M metric tonnes per year in response to the need to improve food security in developing regions of the world and support growing global populations.



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## Wastewater effluents:

- Major source of nutrient inputs to coastal environments
- Most biotechnologies focus on  $\text{NH}_4^+ \rightarrow \text{N}_2$  (*energy intense*)
- Sustainable / energy efficient nutrient recovery strategies are needed





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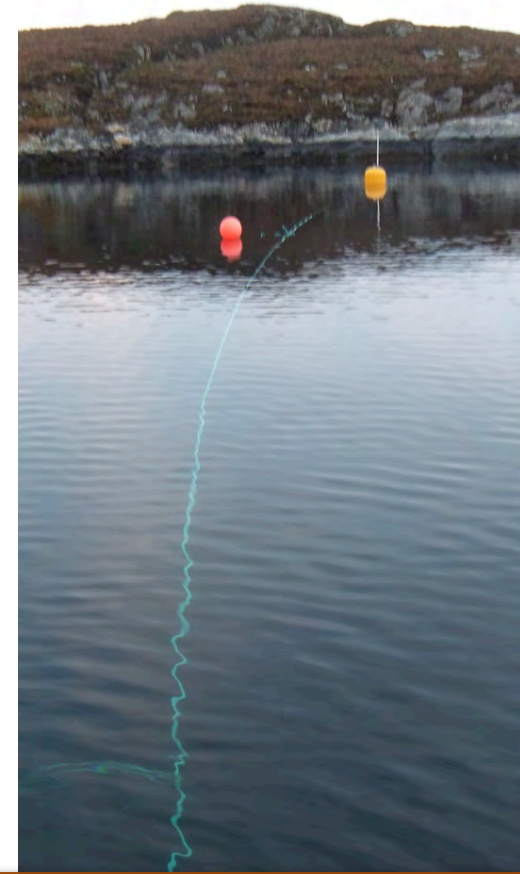
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## Research Goals

- Development of nutrient trading with productive aquaculture as a viable approach to management of the nitrogen cycle in respect to anthropogenic sources of coastal pollution
- Development of biomass feedstock that does not compete for land for food production and that can be supplemented with otherwise wasted nutrients
- Acceleration of the establishment of viable macroalgae aquaculture industry in the US through technology development and greater integration across sectors



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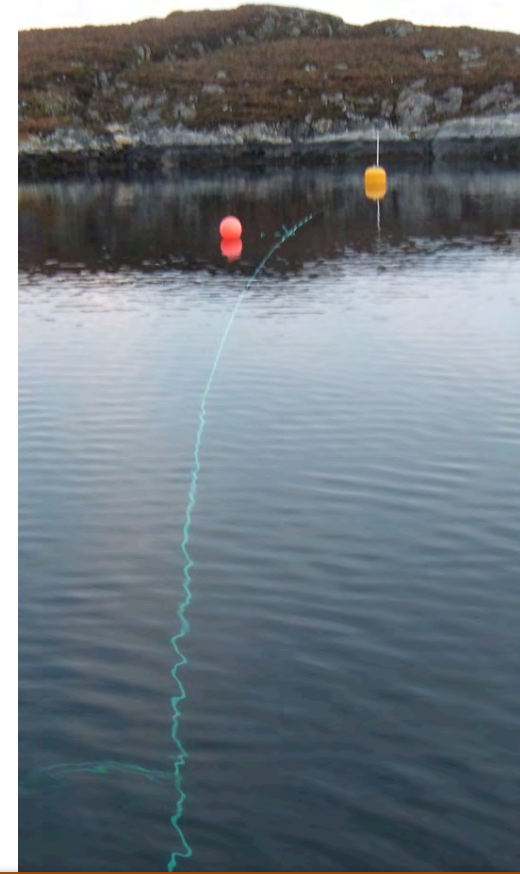
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## Research Objectives

- Determine the nutrient bioextractive potential of *Saccharina latissima* towards application in wastewater treatment plant ocean outfalls
- Determine production area requirements to meet nutrient bioextraction goals for wastewater treatment plants of varying scale and bioprocesses technologies
- Characterize anaerobic digestion potential of the produced kelp and energy recovery as affected by particle size and salinity





# Nutrient bioextraction and bioenergy recovery from ocean outfalls of treatment works

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## Kelp cultivation trials

- *S. latissima* farmed in Boothbay Harbor by Ocean Approved, LLC and the Boothbay Harbor Sanitary District (BHSD) to determine growth rates
- Kelp harvested from Boothbay Harbor in May, 2014.
- Kelp shipped to Clarkson overnight, rinsed with distilled water, and stored frozen until use

Location	Fresh Biomass (ton FW/ha·year)	Dry Biomass (ton DW/ha·year)	Reference
Boothbay Harbor, Atlantic Coast, Maine	45	4.6	This study
Exposed site, Atlantic Coast, Spain	40 ± 3.2	4.7±0.4	Peteiro & Freire, 2013
Sheltered site, Atlantic Coast, Spain	30 ± 2.8	3.5±0.3	Peteiro & Freire, 2013
Sheltered site, West Coast of Sweden	25 (23,28)	5.5 (5.1, 6.2)	Pechsiri et al., 2016
Salmon farm, North Atlantic, Norway	75 (53,88)	11.2 (8.0, 12.9)	Broch et al., 2013



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## Kelp cultivation trials

Biomass characteristics of *S. latissima* cultivated in Boothbay Harbor, Maine, Spring, 2014

Biomass Characteristics*		Tissue Element Contents, mg / g DW					
TS	0.102 g-DW/g-FW	Carbon	305	Aluminum	2.56	Nickel	0.0061
VS	0.742 g-VS/g-DW	Nitrogen	19.0	Arsenic	0.023	Lead	0.0227
COD	116 mg / kg DW	Phosphorus	1.84	Barium	0.031	Selenium	0.0012
GHC	9.8 MJ / kg DW	Potassium	23.0	Cadmium	0.001	Silicon	0.121
BMP <sub>2-ppt</sub>	180 mL / g VS	Calcium	19.2	Cobalt	0.001	Strontium	0.0412
BMP <sub>17-ppt</sub>	110 mL / g VS	Iron	5.89	Chromium	0.007	Titanium	0.119
		Magnesium	8.39	Copper	0.035	Vanadium	0.0119
		Sodium	3.45	Manganese	0.058		
		Sulfur	14.6	Molybdenum	0.001		

\*TS = total solids; VS = volatile solids; COD = chemical oxygen demand; GHC = gross heat of combustion; BMP = biochemical methane potential at a salinity of 2-ppt or 17-ppt

## Annual net nitrogen removal rate: 88 kg /ha • yr

\* Based on 45 ton FW / ha • yr @ 10.2% dry matter

$$\text{Kelp Farm Size (ha)} = \frac{16 \text{ hectares}}{(\text{mg/L N removed}) \cdot (\text{mgd plant flowrate})}$$



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## Wastewater Effluent Goals

Nutrient effluent goals (following Water Environment Federation, 2010)

Level	TN	TP	Comment
1	8.00	1.00	Nominal nutrient removal achievable with conventional technologies
2	3.00	0.10	Enhanced removal: requires additional treatment to achieve limits
3	1.00	0.01	Very low limits: requires best practices and enhanced treatment. May or may not be feasible for some plants, especially requiring both limits simultaneously.



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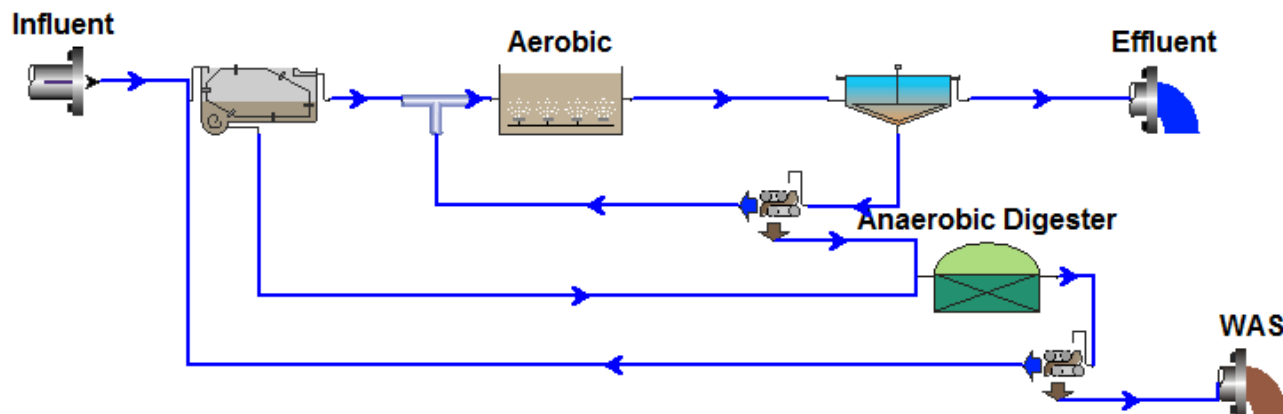
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## System Integration: Secondary Treatment

Modeled effluent characteristics for an activated sludge treatment assuming midline influent characteristics and bioprocess kinetics

Parameter	Influent §	Effluent
pH	7.00	6.98
Alkalinity, mg/L	100.00	82.00
Dissolved Oxygen, mg/L	2.00	2.00
Biochemical Oxygen Demand, mg/L	190.00	24.30
Total Suspended Solids, mg/L	210.00	14.00
Volatile Suspended Solids, mg/L	160.00	9.40
Total Nitrogen, mg/L	40.00	<b>9.60</b>
Total Phosphorus, mg/L	7.00	4.40

§ Midline characteristics (Metcalf & Eddy, Wastewater Engineering Treatment & Reuse, 2003, Fourth Edition)





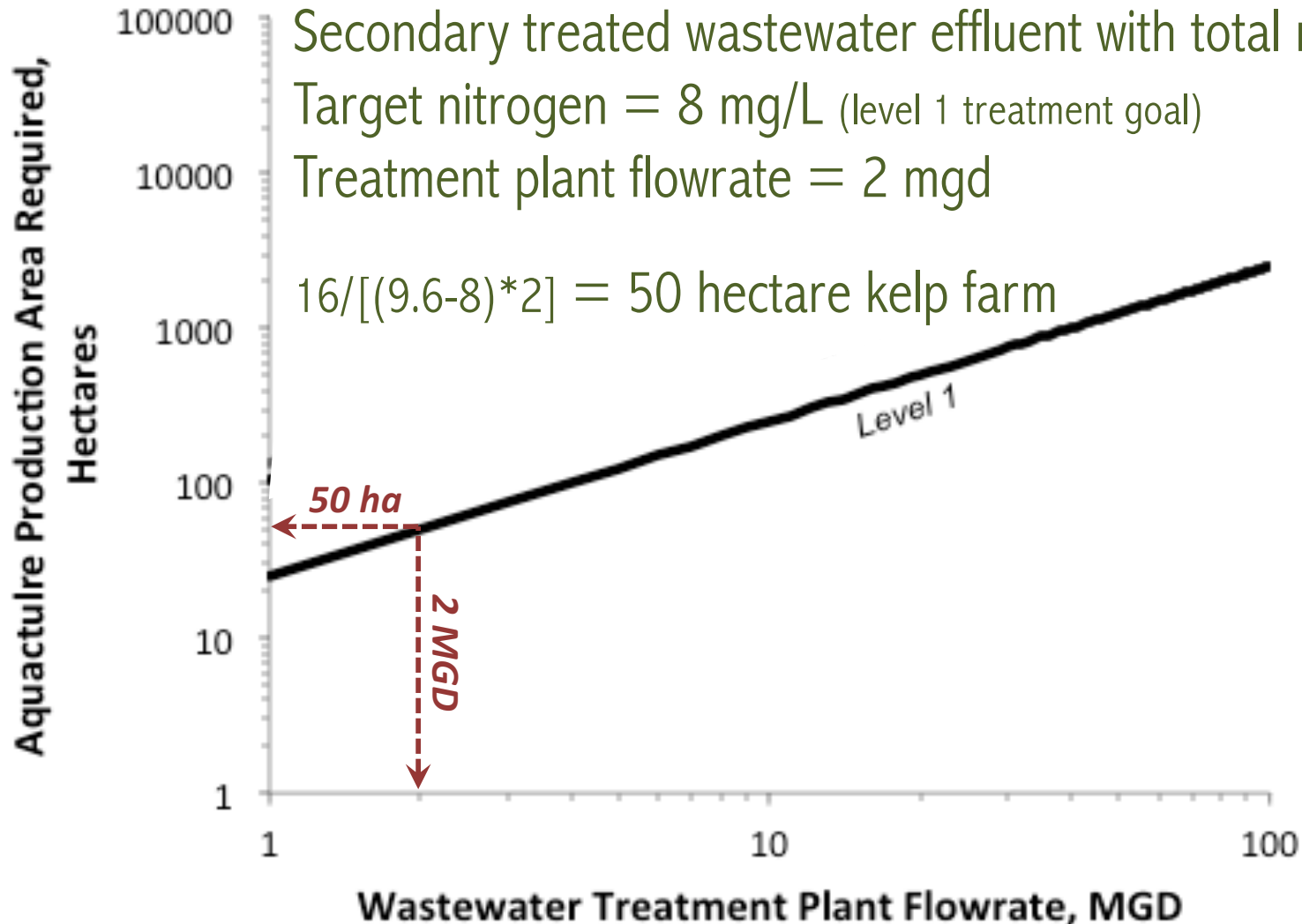
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## System Integration: Secondary Treatment + *S. latissima* Cultivation



Estimated production area requirements for *S. latissima* aquaculture to achieve nitrogen removal goals following secondary treatment by activated sludge in WWTPs of varying size.

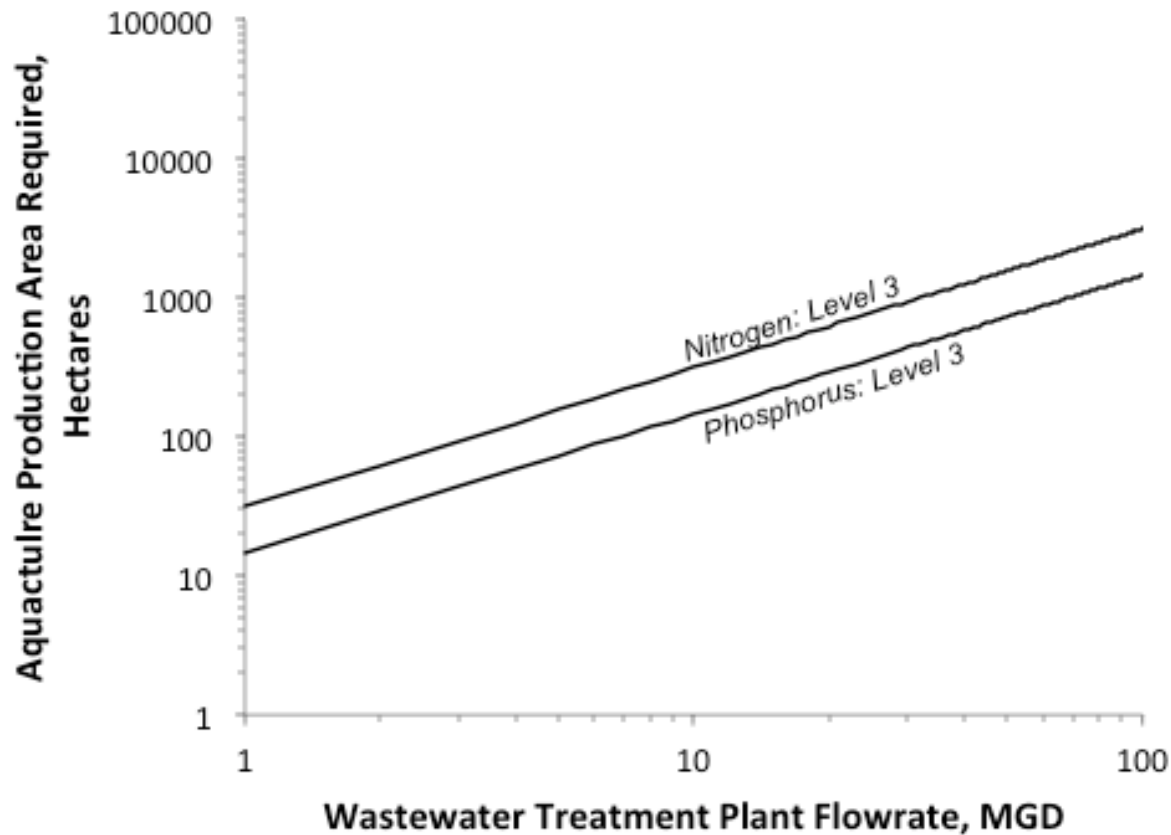
# Nutrient bioextraction and bioenergy recovery from ocean outfalls of treatment works

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## System Integration: Tertiary Treatment + *S. latissima* Cultivation



Estimated production area requirements for *S. latissima* aquaculture to achieve level 3 nutrient removal goals following tertiary treatment (various processes) to meet level 2 nutrient effluent goals, in WWTPs of varying size.



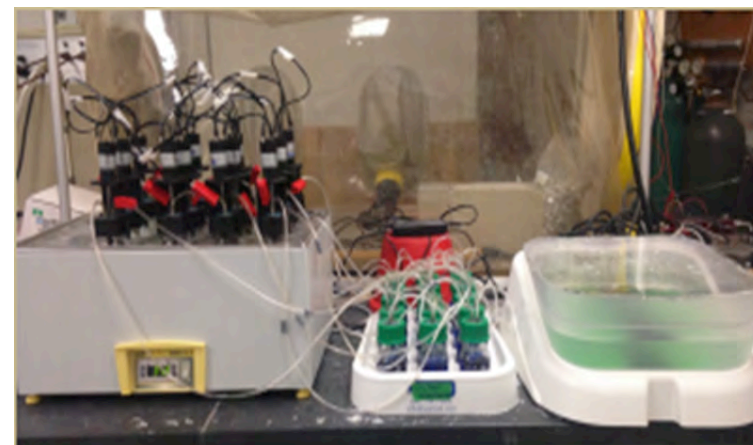
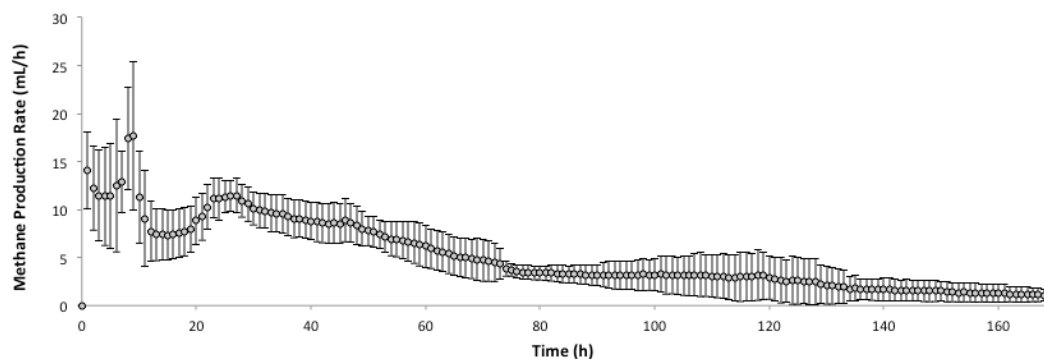
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## Biomethane Potential



Species	Category	BMP (mL/g VS)	Reference
<i>Saccharina latissima</i>	Brown algae	180 ± 17	This study
<i>Saccharina latissima</i>	Brown algae	440*	Pechsiri et al., 2016
Overall macroalgae		140 - 400	Murphy et al., 2013
<i>Saccharina latissima</i>	Brown algae	260 - 280	Chynoweth et al., 1993b
<i>Macrocystis</i>	Brown algae	390 - 410	
<i>Gracilaria</i>	Red algae	280 - 400	
<i>Sargassum</i>	Brown algae	260 - 380	
<i>Ulva lactuca</i>	Green algae	162 - 271	

\* 180 mL/g VS was used in subsequent calculations as a conservative estimate

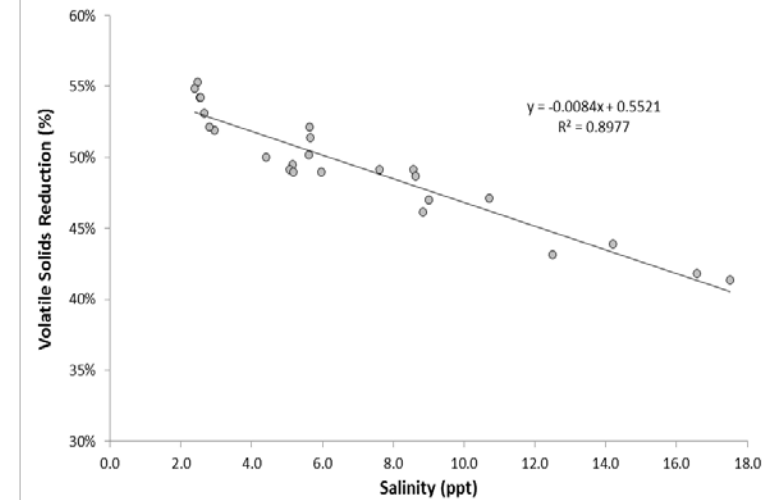
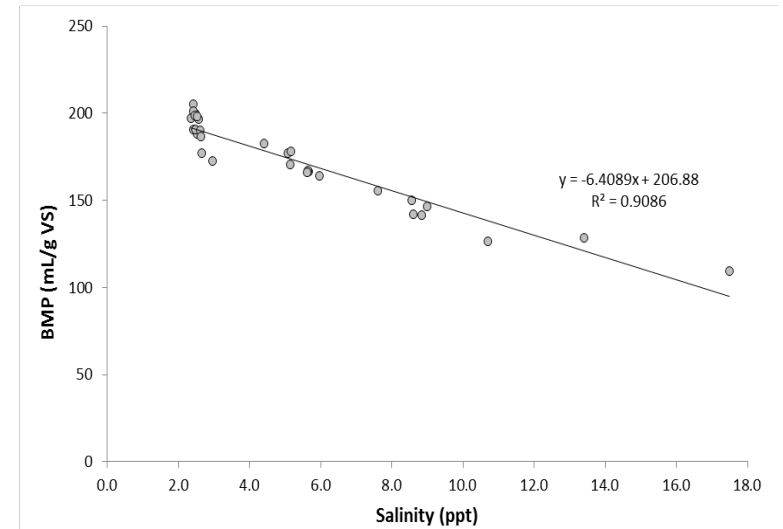
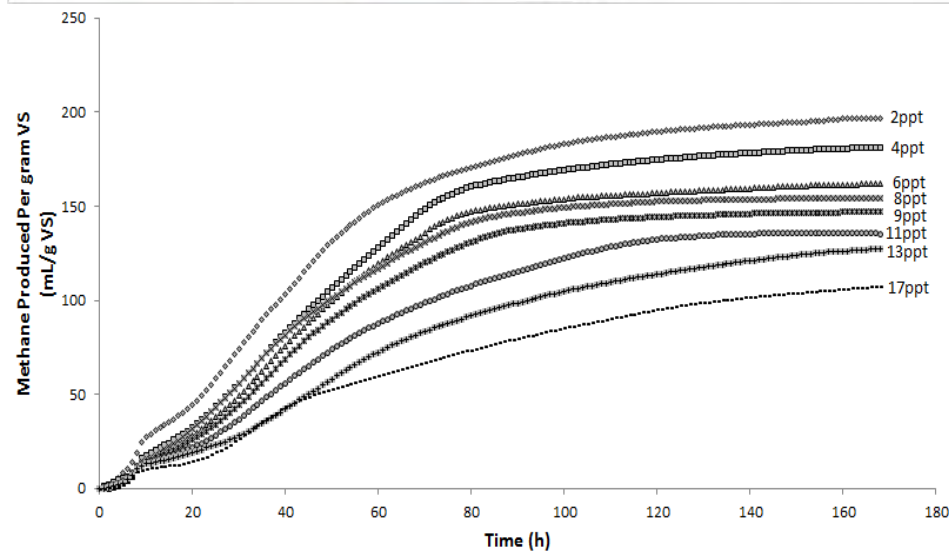
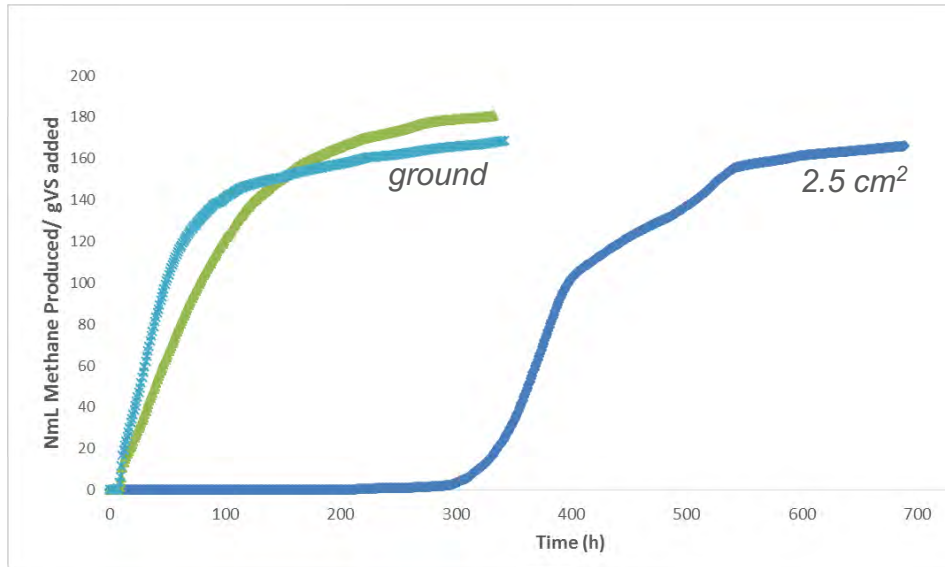
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## Biomethane Potential: Effects of Particle Size and Salinity





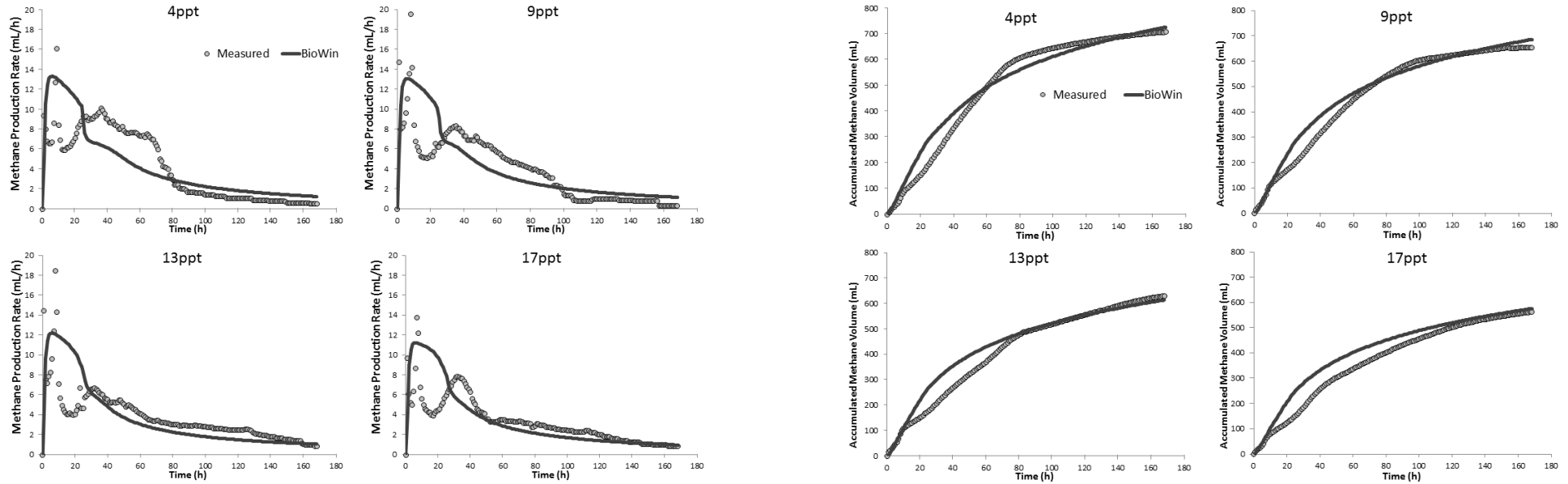
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## Biomethane Potential: Best Fit Rate Coefficients



Salinity (ppt)	Anaerobic Hydrolysis factor	Hydrolysis rate (d <sup>-1</sup> )	Anaerobic decay rate (d <sup>-1</sup> )	Fermentation rate (d <sup>-1</sup> )	Acetoclastic max spec. growth rate (d <sup>-1</sup> )	H <sub>2</sub> utilizing growth rate (d <sup>-1</sup> )
2	1.8	0.7	0.13	1.6	0.27	1.4
4	1.8	0.7	0.13	1.6	0.14	1.4
9	1.8	0.7	0.13	1.4	0.12	1.4
13	1.8	0.65	0.13	1.3	0.09	1.3
17	1.8	0.65	0.12	1.1	0.06	1.1
24	1.8	0.52	0.08	0.9	0.01	0.4
27	1.8	0.45	0.06	0.7	0.01	0.37

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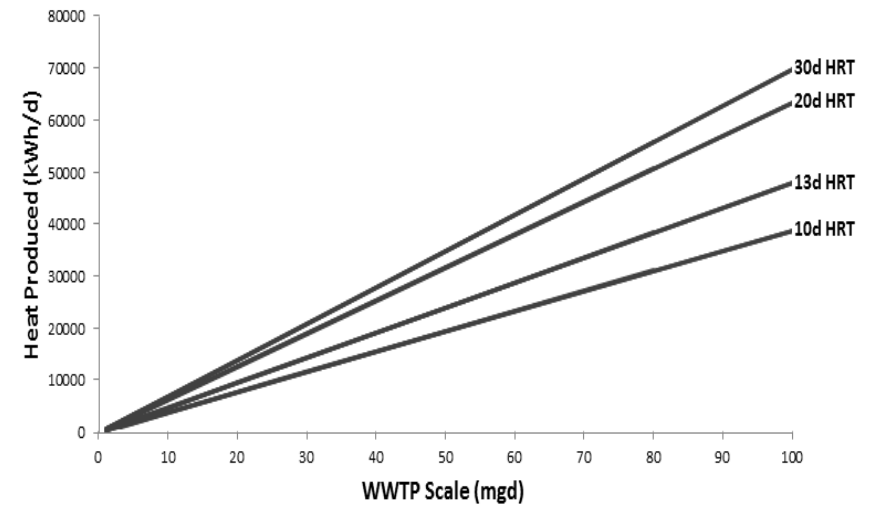
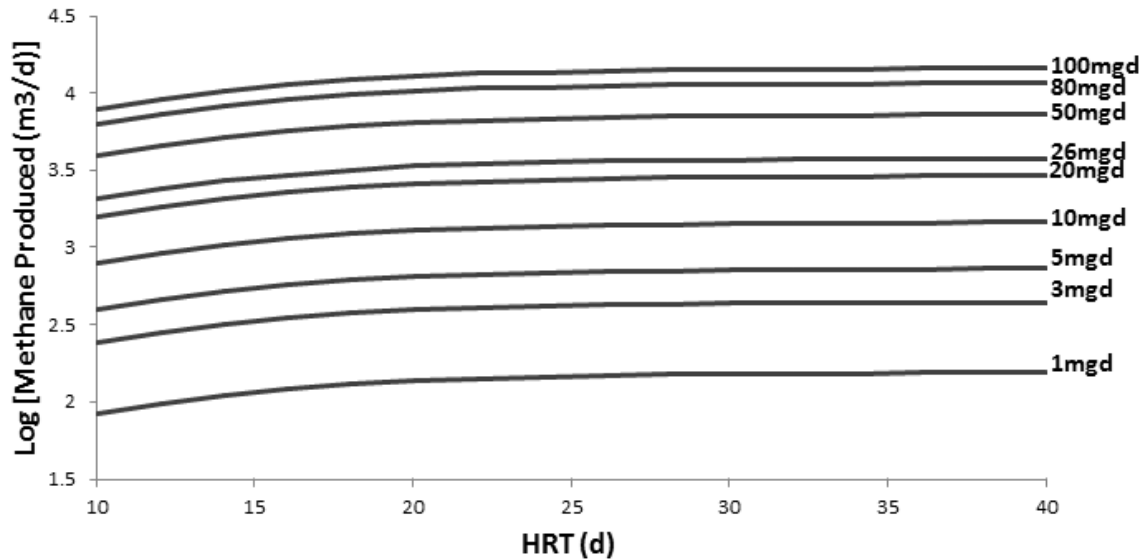
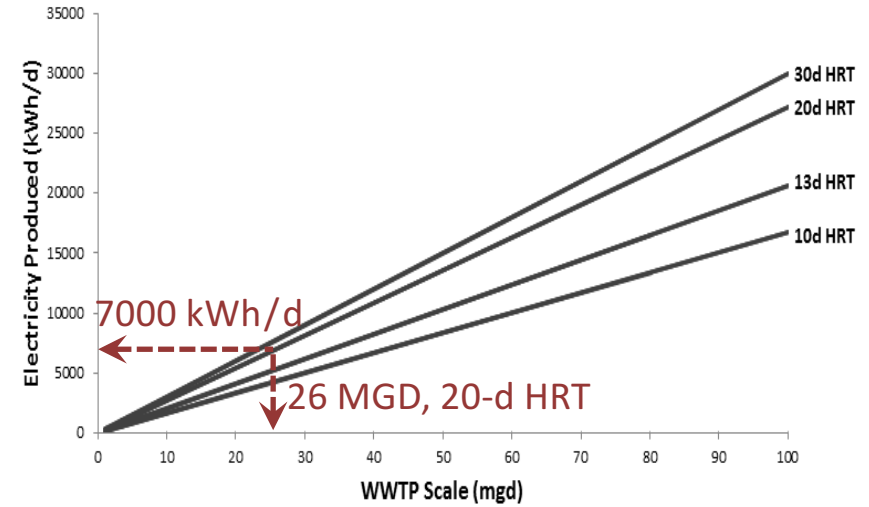
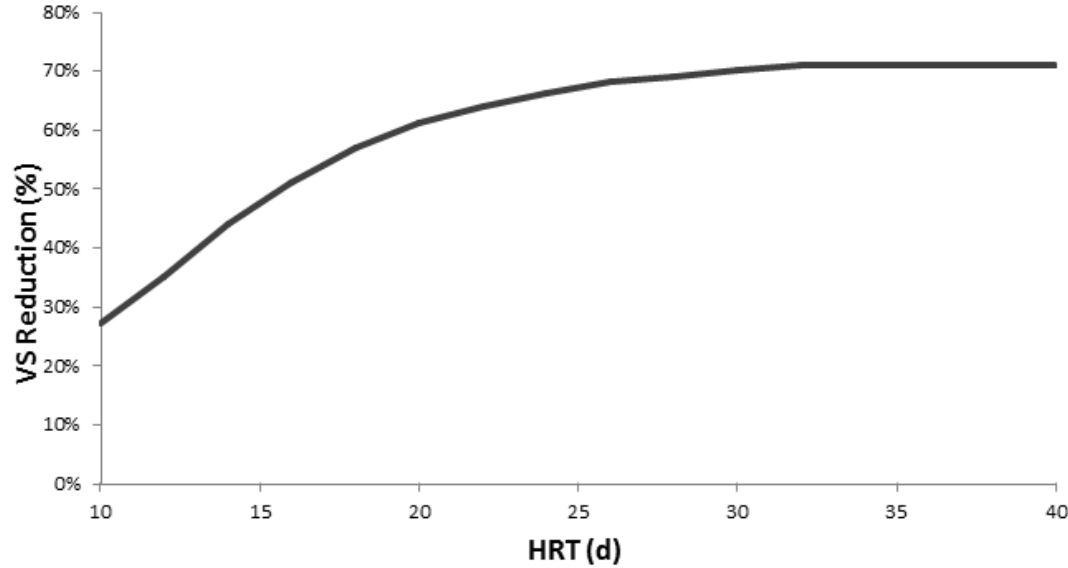
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## Biomethane Potential: Full-scale anaerobic digestion simulations

*Based on 45 ton FW/ha·year*



## Discussion and Conclusions

- *S. latissima* was explored for potential nutrient bioextraction and recovery from plumes of ocean outfalls of WWTPs.
  - 45 tons FW/ha
  - Biomass production characteristics may be greater when grown in nutrient-rich plumes
  - 88 kg-N/ha • yr
  - Composition may be affected by period of harvest
  - 16 ha / [(mg/L N removed)(mgd)]
- Macroalgae aquaculture for nutrient recovery and biomass production may be a viable alternative, especially for smaller wastewater treatment plants and those seeking very low levels of net nutrients discharge in conjunction with tertiary treatment processes
- Biomethane potential of *S. latissima* was 180 mL CH<sub>4</sub>/g VS
  - Strongly influenced by salinity
  - Pretreatment may be necessary for effective anaerobic digestion.
  - Alternative anaerobic digester seeds (potential for greater biomethane production)
  - Harvesting period may play a role



## Continuing Work

- Exploration of effects of growth in plumes of wastewater discharges on kelp production rates and biomass composition.
  - Positive effects of nutrients enrichment on growth and composition may be offset by negative effects of increased micropollutants, turbidity, DOM, etc.
  - Biomass characteristics may be influenced by growth and harvesting periods
  - WWTP effluent quality and composition of nutrients will change with seasons
- Analysis of the technology as a component of wastewater treatment practice will help understand economic benefits and trade-offs relative to tertiary treatment. Mixture of goods that may emerge from *S. latissima* (e.g., proteins, alginates, succinic acid, phenols...) should be explored.
- Life cycle assessment of the proposed process as an alternative to nutrient removal by engineered operations and processes

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